DEVELOPMENT AND CHARACTERIZATION OF NOVEL HERBAL FORMULATION (POLYMERIC MICROSPHERES) OF SYZYGIUM CUMINI SEED EXTRACT

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ABSTRACT

Objective: The purpose of the present investigation was to develop and characterize a novel herbal formulation (polymeric microspheres) of Syzygium cumini seed extract.

Methods: The extract-loaded microspheres using biological macromolecule ethyl cellulose (EC) was prepared by o/w emulsion solvent evaporation technique using polyvinyl alcohol (PVA) emulsifier. The effect of various process and formulation variables (stirring speed, evaporation time, drug/polymer ratio and organic/aqueous phase ratio) on the properties of microspheres was evaluated.

Results: Micromeritic properties indicated good flow properties, and scanning electron microscopy (SEM) confirmed the spherical nature of the prepared microspheres. The particle size and entrapment efficiency were varied between 34.25 to 176.25 µm and 10.51 to 42% depending upon the variables. All the formulations showed minimal drug release in an acidic environment (pH 1.2) confirming the prevention of drug release in the stomach and enteric nature of the polymer. Sustained drug release has been observed in alkaline dissolution media (pH 7.4) after 12 h of drug release study except for formulation F7 which contains a lower concentration of polymer. The fourier transform infrared spectroscopy (FTIR) analysis indicated the compatibility of the extract with the polymer. The absence of extract-polymer interaction was indicated by the differential scanning calorimetry (DSC) thermogram. x-ray diffraction (XRD) analysis revealed the amorphous nature of the extract in the microspheres which in pure form exhibits a crystalline structure.

Conclusion: The findings of this present study suggest that microsphere formulation was a promising carrier for novel delivery of herbal drugs.

Keywords: Polymeric microspheres, Ethylcellulose, Syzygium cumini, Herbal formulation, Solvent evaporation, Polyvinyl alcohol, Phytopharmaceuticals, Novel drug delivery system

INTRODUCTION

Herbal medicines are the oldest form of health care and the future of medicine is rooted in the past. Herbs are staging a comeback and herbal "renaissance" is happening all over the globe. People are being interested in herbal therapies rather mainstream medicine due to there is a growing concern over the reliance and safety of drugs and surgery as well as many natural measures produce better results than drugs/surgery without the side effects [1]. Diabetes mellitus (DM), the third "killer" of mankind, is an important chronic metabolic disorder (also called lifestyle disease) affecting carbohydrate, protein and fat metabolism. The worldwide survey reported that the DM is affecting nearly 10% of the populations. The diabetic people are not able to produce or properly use insulin in the body, so they have a high level of blood glucose. DM is managed by oral hypoglycemic agents which have a characteristic profile of serious side effects [2]. So, despite considerable progress in the management of DM by synthetic drugs, the search for indigenous natural antidiabetic agents is still going on. Ethnobotanical information also indicates that more than 800 plants are used as traditional remedies for the treatment of diabetes throughout the world [3]. Recently herbal medicines have acquired more importance in the treatment of diabetes as they are free from side effects and less expensive when compared to synthetic hypoglycemic agents [4]. Syzygium cumini (L.) seed which is rich in polyphenols and flavonoids, has been reported to be widely used as the traditional system of medicine to treat diabetes [5]. Conventional formulation (powder dosage form) of Syzygium cumini seed is available commercially and the diabetic people widely use it to regulate their blood glucose level. Drugs of natural origin suffer from poor physicochemical properties, which are related to their poor bioavailability, diminishing their therapeutic potency despite their extraordinary potential [6]. Generally to overcome these limitations, developing the novel herbal drug delivery system (NHDDS) with better absorption profile is of premier importance [1]. These novel formulations are advantageous over conventional formulations regarding enhancement of solubility, stability, membrane permeability, bioavailability, improved pharmacological activity through sustained release profile and reduced toxicity [6]. The novel carriers firstly, deliver the drug at a predetermined rate over the period of treatment and secondly, channel the active entity to the site of action. Whereas the conventional dosage forms are unable to achieve these. Micro/nano-sized NHDDS have a potential future for enhancing the activity and overcoming problems associated with plant medicines [1].

In the past, herbal drugs did not attract researcher's interest in the development of NDDS due to difficulties in processing (including standardization, extraction, and identification). However, with the advancement of modern scientific techniques, recently new doors have been opened for the development of novel herbal formulation [7]. Today one of the most attractive areas of research in drug delivery is the design of polymeric microspheres that are able to deliver the drug to the target site, at the right time and right doses [8]. Ethyl cellulose is a semi-synthetic, lipophilic, non-toxic, biocompatible, non-degradable, cost-effective polymer and has been widely used for both lipophilic and hydrophilic drugs in the preparation of controlled release dosage form. Among all other methods used to prepare microspheres, solvent evaporation technique is the simplest one [9].

No attempts have been made for the development of the novel formulation of Syzygium cumini seed extract. In this study, we have tried to develop a smart delivery system for the extract. So, the objective of the present work was to develop and characterize novel herbal formulation (polymeric microspheres) of Syzygium cumini seed extract by emulsion solvent evaporation technique using ethyl cellulose as the polymer.
MATERIALS AND METHODS

Materials

_Syzgium cumini_ seed powder (Vyas Pharmaceuticals, a GMP certified unit, Indore, MP, India), Ethylcellulose (Loba Chemie Pvt. Ltd.), Polyvinyl alcohol (Nice Chemicals P Ltd.), Dichloromethane (Loba Chemie Pvt. Ltd.). All other chemicals used were of analytical grade.

Preparation of extract

The _Syzgium cumini_ seed powder was extracted with ethanol-water (70:30) at room temperature by maceration for 14 d. The extract was then filtered and concentrated by a rotary vacuum evaporator at a temperature of 40°C. It was then kept in the refrigerator in an airtight container for further studies.

Preparation of extract-loaded ethyl cellulose microspheres

Extract-loaded polymeric microspheres were prepared at room temperature by most widely used o/w emulsion solvent evaporation technique [10, 11]. Different formulations were prepared by dissolving the polymer and drug in dichloromethane (DCM) as specified in table 1. This polymeric drug solution (internal oil phase) was emulsified by pouring slowly into external aqueous phase containing 1% w/v polyvinyl alcohol (PVA) as an emulsifying agent, with continuous stirring using propeller type electric stirrer (Remi, Mumbai, India). The stirring speed and evaporation time were specified in table 1. During the emulsification process, the dispersed phase was converted into minute droplets and then solidified into rigid microspheres due to evaporation of the organic solvent. The resulting microspheres were recovered by filtration, washed three times with double distilled water to remove any residual PVA and dried at room temperature. All the formulations were prepared in triplicate and further characterized.

Characterization of microspheres

Production yield

After drying the obtained microspheres were weighed accurately. The % yield was determined by using the following formula:

\[
\%\text{yield} = \frac{\text{Mass of microspheres obtained}}{\text{Total mass of drug + polymer}} \times 100
\]

Table 1: Formulation design of extract-loaded ethyl cellulose microspheres

<table>
<thead>
<tr>
<th>Batch code</th>
<th>Stirring speed (rpm)</th>
<th>Evaporation time (h)</th>
<th>Drug/polymer ratio</th>
<th>Organic/aqueous phase ratio</th>
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<tr>
<td>F1</td>
<td>800</td>
<td>3</td>
<td>1:2</td>
<td>1:3</td>
</tr>
<tr>
<td>F2*</td>
<td>1000</td>
<td>3</td>
<td>1:2</td>
<td>1:3</td>
</tr>
<tr>
<td>F3</td>
<td>1500</td>
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<tr>
<td>F4</td>
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<td>1</td>
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<td>1:3</td>
</tr>
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<td>3</td>
<td>1:2</td>
<td>1:3</td>
</tr>
<tr>
<td>F7</td>
<td>1000</td>
<td>3</td>
<td>1:1</td>
<td>1:3</td>
</tr>
<tr>
<td>F8*</td>
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<tr>
<td>F9</td>
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<tr>
<td>F12</td>
<td>1000</td>
<td>3</td>
<td>1:2</td>
<td>1:10</td>
</tr>
</tbody>
</table>

*Same formulation variables.

Drug entrapment efficiency (DEE)

Entrapment efficiency was determined by dissolving 10 mg of microspheres in 2 ml DCM. When the particles were completely dissolved, the mixture was diluted up to 50 ml with phosphate buffer pH 7.4 and stirred for 1 h by using a magnetic stirrer for complete removal of DCM. The polymer was removed by filtration. The absorbance of the filtrate was measured at 760 nm, and the content was determined by dissolving the polymer and drug in dichloromethane (DCM) as specified in table 1. This polymeric drug solution (internal oil phase) was emulsified by pouring slowly into external aqueous phase containing 1% w/v polyvinyl alcohol (PVA) as an emulsifying agent, with continuous stirring using propeller type electric stirrer (Remi, Mumbai, India). The stirring speed and evaporation time were specified in table 1. During the emulsification process, the dispersed phase was converted into minute droplets and then solidified into rigid microspheres due to evaporation of the organic solvent. The resulting microspheres were recovered by filtration, washed three times with double distilled water to remove any residual PVA and dried at room temperature. All the formulations were prepared in triplicate and further characterized.

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\[
\text{% Drug entrapment} = \frac{\text{Calculated drug content}}{\text{Theoretical drug content}} \times 100
\]

Micromeritic properties

Bulk density

A measured quantity of microspheres was introduced into 10 ml measuring cylinder, and the volume was noted. After that, it was tapped manually 100 times. Again the volume was noted. The loose and tapped bulk density was determined by using the following formulas

\[
\text{Loose bulk density (LBD)} = \frac{\text{Weight of microspheres}}{\text{Bulk volume}}
\]

\[
\text{Tapped bulk density (TBD)} = \frac{\text{Weight of microspheres}}{\text{Tapped volume}}
\]

Carr’s index

Indirect measurement of rheological properties like shape, size, surface area, moisture content and cohesiveness of materials is done by using Carr’s index. It is also known as Carr’s compressibility index (Ci).

\[
\text{Carr’s index} = \frac{\text{Tapped density – bulk density}}{\text{Tapped density}} \times 100
\]

It reflects the flow characteristics of materials. 

Hausner’s ratio

Another index for measuring flowability of materials.

\[
\text{Hausner’s ratio (H)} = \frac{\text{Tapped density}}{\text{Bulk density}}
\]

Angle of repose

The maximum possible angle between the surface of the pile and the horizontal plane is known as the angle of repose. It was determined by the fixed funnel method using the following formula:

\[
\tan \theta = \frac{h}{r}
\]

Where,

- \( h \) = height of the pile
- \( r \) = radius of the pile

Particle size analysis

The particle size of the prepared microspheres was measured by the optical microscope with the aid of an eye-piece micrometer which was previously calibrated with the stage micrometer. The mean particle size and size distribution were determined.
**In vitro drug release studies**

The drug release profile of formulated microspheres was carried out by using USP dissolution test apparatus type II rotating paddle. The test was performed both in 0.1 N HCl (pH 1.2) and phosphate buffer (pH 7.4) as dissolution media (900 ml) maintained at 37±0.5 °C and 100 rpm. The samples were withdrawn at predetermined time intervals, filtered and analyzed spectrophotometrically at 760 nm. Cumulative % drug release (CPR) was calculated from the standard curve.

**Drug-excipients interaction study by FTIR**

The FTIR spectra were taken to investigate the possible interaction between drug and polymer in the microspheres formulation. The spectra of the extract, polymer, empty microspheres and extract-loaded microspheres were recorded in the range of 4000-400 cm⁻¹ for the FTIR spectra. The FTIR spectra were taken to investigate the possible interaction by FTIR of the drug and that of the formulation. The loaded microspheres were recorded in the range of 4000 -400 cm⁻¹.

**Surface morphology of microspheres (SEM)**

Scanning electron microscopy is an excellent tool to examine the shape and surface morphology of the microspheres. Prior to observation, the sample was placed on an adhesive stub. The SEM photograph was taken at a working distance of 15 mm; the acceleration voltage is 15 kV with secondary electron image (SEI) detector.

**X-ray diffraction analysis (XRD)**

The XRD pattern of the extract and the microspheres were obtained by X-ray diffractometer. The samples were irradiated with monochromatized X-ray (Cu Kα) with scanning rate of 2°min⁻¹ in the range of 5-70 °C (2θ diffraction angle). The voltage was 40 kV and current 30mA.

**Drug release kinetics studies**

Drug release mechanism from the microspheres was studied by fitting the in vitro release data of optimized formulation to different mathematical models such as Zero order (% cumulative drug release vs. time), first order (log % drug retained vs. time), Higuchi model (% cumulative drug release vs. square root of time) and Peppas exponential equation (log % drug release vs. log time). All curve fitting, calculation, and plotting were performed using Microsoft excel solver, and regression coefficient (R²) values were calculated.

**RESULTS AND DISCUSSION**

**Formulation of microspheres**

The solvent evaporation method, most common and patented, was selected for the preparation of ethyl cellulose microspheres for novel delivery of Syzygium cumini seed extract. Though the method is simple, many factors have been shown to influence the properties of the prepared microspheres [12]. Size is one of the most important factors that should be considered in the design and development of this system as size affects the interaction with the biological system, entry of the drug and drug release. Another important parameter is the entrapment efficiency (EE) which in turn related to the productivity of the pharmaceutical system [13]. The extract loaded ethyl cellulose microspheres were prepared successfully by o/w emulsion solvent evaporation method. Microspheres were formed by pouring a polymeric drug solution in dichloromethane, into the aqueous solution of PVA. The evaporation of entrapped dichloromethane leads to the formation of microspheres [14]. This formed smooth surfaced, spherical shaped microspheres. All the batches were prepared according to the formulation design (table 1). The desirable characteristics of the prepared microspheres are high EE, small particle size, and controlled drug release. As various formulation and processing variables influenced the properties of microspheres, the present work focused towards the systematic investigation of the parameters which could influence the microspheres characteristics. Gallic acid was used as a marker peak for Jamun and its formulations [15].

**Production Yield**

The percentage yield for all the formulations was found to be in the range of 39.53-58.79% (table 2) and it was increasing with increased polymer concentration and evaporation time. It decreased when the external aqueous phase volume increased. When the stirring rate was increased from 800 to 1000 rpm, % yield increased (52.23-54.75%), but on further increase in the rate to 1500 rpm, it decreased [16, 17].

**Micromeritic properties**

The micromeritic properties for all the formulations were expressed in terms of bulk density, tapped density, Carr's index, Hausner’s ratio and angle of repose. As given in table 2, the values of Carr's index were found to be in the range of 1.13-15.66%, indicating good compressibility. Hausner's ratio was recorded below 1.25, which represents good flowability. The angle of repose was found to be below 30°, showing the free-flowing nature of the microspheres. The micromeritic properties of all the formulations indicated that microspheres were free flowing in nature. The similar finding was also reported previously [9, 16].

**Table 2: Production yield and flow properties of extract-loaded ethyl cellulose microspheres**

<table>
<thead>
<tr>
<th>Batch code</th>
<th>% yield</th>
<th>Bulk density (g/ml)</th>
<th>Tapped density (g/ml)</th>
<th>Carr's index (%)</th>
<th>Hausner’s ratio</th>
<th>Angle of repose (°)</th>
</tr>
</thead>
<tbody>
<tr>
<td>F1</td>
<td>52.23</td>
<td>0.45±0.42</td>
<td>0.51±0.13</td>
<td>11.13</td>
<td>1.12</td>
<td>18.53±0.62</td>
</tr>
<tr>
<td>F2</td>
<td>54.75</td>
<td>0.13±0.59</td>
<td>0.175±0.15</td>
<td>12.57</td>
<td>1.14</td>
<td>20.12±0.73</td>
</tr>
<tr>
<td>F3</td>
<td>45.23</td>
<td>0.11±0.32</td>
<td>0.13±0.21</td>
<td>14.71</td>
<td>1.17</td>
<td>22.57±0.55</td>
</tr>
<tr>
<td>F4</td>
<td>42.35</td>
<td>0.149±0.15</td>
<td>0.16±0.35</td>
<td>11.31</td>
<td>1.13</td>
<td>21.44±0.63</td>
</tr>
<tr>
<td>F5</td>
<td>49.69</td>
<td>0.13±0.40</td>
<td>0.15±0.51</td>
<td>15.18</td>
<td>1.18</td>
<td>23.97±0.81</td>
</tr>
<tr>
<td>F6</td>
<td>54.75</td>
<td>0.15±0.29</td>
<td>0.175±0.34</td>
<td>12.57</td>
<td>1.14</td>
<td>20.12±0.93</td>
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<tr>
<td>F7</td>
<td>40.31</td>
<td>0.17±0.31</td>
<td>0.17±0.43</td>
<td>14.04</td>
<td>1.16</td>
<td>23.56±0.57</td>
</tr>
<tr>
<td>F8</td>
<td>54.75</td>
<td>0.15±0.42</td>
<td>0.175±0.33</td>
<td>12.57</td>
<td>1.14</td>
<td>20.12±0.75</td>
</tr>
<tr>
<td>F9</td>
<td>58.79</td>
<td>0.218±0.23</td>
<td>0.256±0.36</td>
<td>14.94</td>
<td>1.17</td>
<td>24.31±0.79</td>
</tr>
<tr>
<td>F10</td>
<td>54.75</td>
<td>0.15±0.51</td>
<td>0.175±0.25</td>
<td>12.57</td>
<td>1.14</td>
<td>20.12±0.61</td>
</tr>
<tr>
<td>F11</td>
<td>42.21</td>
<td>0.16±0.23</td>
<td>0.195±0.19</td>
<td>13.33</td>
<td>1.15</td>
<td>24.92±0.57</td>
</tr>
<tr>
<td>F12</td>
<td>39.53</td>
<td>0.18±0.29</td>
<td>0.217±0.35</td>
<td>15.66</td>
<td>1.19</td>
<td>25.14±0.73</td>
</tr>
</tbody>
</table>

Data represent mean±standard deviation (SD), n=3.

**Drug entrapment efficiency (DEE)**

All the formulations were evaluated for entrapment efficiency (EE), and the results are illustrated in table 3, which shows that the polymer concentration and evaporation time are directly proportional to the EE, whereas the stirring speed and organic/aqueous phase volume ratio are inversely proportional to the EE [18]. High polymer concentration increases the viscosity of the organic phase, which increases the diffusion resistance to the drug molecules, thereby reducing the partitioning of the drug into
external aqueous phase and entrapping more drug in polymeric microspheres [12]. In another way, with the increase in polymer concentration, the particle size increases. This causes the decrease in the surface area to be exposed to water. Thus, the drug loss due to diffusion is reduced and enhanced entrapment [13]. As the drug: polymer ratio increased from 1:1 to 1:2 and 1:3, the mean EE increased from 18% to 30.03% and 42% respectively. Evaporation of organic solvent for the shorter period of time causes rapid replacement of the organic solvent with the aqueous medium before the droplet hardening occurs. This results in reduced drug entrapment. The lowest entrapment (15.01%) was observed when the evaporation time was 1h. Upon increasing the aqueous phase volume, more amount of drug is dissolved in the aqueous medium. Therefore, increasing the drug loss from organic phase results in the reduction of the EE [19]. An increase in the particle size was observed with increased organic/aqueous phase ratio which may be explained by the change in viscosity of the emulsion formed during the process. Increased viscosity resulted in high viscous resistance against the shear force during the microparticle formation. The external energy (in the form of stirring speed and amount of emulsifier) for droplet breakdown was kept constant. Thus, on increasing the aqueous phase volume, the same amount of energy must be distributed in large volume, causing less droplet breakdown and resulting larger particles. When the stirring rate was increased from 800 to 1500 rpm, the particle size was reduced rapidly (176.25-38.5 µm). This is because higher energy is released in the process that leads to the rapid breakdown of the emulsion droplets, resulting in smaller particle size [19]. The particle size distribution of the optimized formulation was shown in fig. 2. 

**Particle size**

The particle size was determined by optical microscopy using eyepiece micrometer which was previously calibrated with the stage micrometer. The particle size was measured in the range of 34.25-176.25 µm among different formulations. The mean particle size of the microspheres significantly increased (34.25 to 114.75 µm) with an increase in polymer concentration. Higher polymer concentration with the fixed volume of organic solvent causes more viscous dispersion, leading to the formation of larger emulsion droplet and consequently larger particles. The viscous forces oppose the shear stresses in the organic phase, and the final particle size depends on the net shear stress available for droplet breakdown [21]. A critical parameter determining the particle size is diffusion of the organic solvent through the interface of emulsion droplet. For shorter evaporation time, the diffusion may not have been completed before the droplets start to harden, thus forming larger particles. But when the organic solvent is allowed to evaporate for a long time, the extent of diffusion will be greater, resulting in a smaller particle size. An increase in the particle size was observed with increased organic/aqueous phase ratio which may be explained by the change in viscosity of the emulsion formed during the process. Increased viscosity resulted in high viscous resistance against the shear force during the microparticle formation. The external energy (in the form of stirring speed and amount of emulsifier) for droplet breakdown was kept constant. Thus, on increasing the aqueous phase volume, the same amount of energy must be distributed in large volume, causing less droplet breakdown and resulting larger particles. When the stirring rate was increased from 800 to 1500 rpm, the particle size was reduced rapidly (176.25-38.5 µm). This is because higher energy is released in the process that leads to the rapid breakdown of the emulsion droplets, resulting in smaller particle size [19]. The particle size distribution of the optimized formulation was shown in fig. 2.

**Table 3: Comparison of entrapment efficiency, particle size and the cumulative amount of drug release from extract-loaded ethyl cellulose microspheres prepared using various process and formulation variables**

<table>
<thead>
<tr>
<th>Batch code</th>
<th>Entrapment efficiency (%±SD)</th>
<th>Mean particle size (µm±SD)</th>
<th>Cumulative drug release at 12h (%±SD)</th>
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</thead>
<tbody>
<tr>
<td>F1</td>
<td>39.03±2.6</td>
<td>176.25±58.4</td>
<td>62.30±1.2</td>
</tr>
<tr>
<td>F2</td>
<td>30.03±2.1</td>
<td>45.5±26.4</td>
<td>88.30±0.8</td>
</tr>
<tr>
<td>F3</td>
<td>19.5±1.9</td>
<td>38.5±20.8</td>
<td>92.50±1.6</td>
</tr>
<tr>
<td>F4</td>
<td>15.01±3.6</td>
<td>128.5±43.1</td>
<td>61.20±2.1</td>
</tr>
<tr>
<td>F5</td>
<td>25.5±2.9</td>
<td>87.5±35.1</td>
<td>72.47±1.1</td>
</tr>
<tr>
<td>F6</td>
<td>30.03±2.1</td>
<td>45.5±26.4</td>
<td>88.30±0.8</td>
</tr>
<tr>
<td>F7</td>
<td>18.00±4.3</td>
<td>34.5±23.7</td>
<td>99.22±1.8*</td>
</tr>
<tr>
<td>F8</td>
<td>30.03±2.1</td>
<td>45.5±26.4</td>
<td>88.30±0.8</td>
</tr>
<tr>
<td>F9</td>
<td>42.00±1.9</td>
<td>114.75±45.9</td>
<td>56.19±2.0</td>
</tr>
<tr>
<td>F10</td>
<td>30.03±2.1</td>
<td>45.5±26.4</td>
<td>88.30±0.8</td>
</tr>
<tr>
<td>F11</td>
<td>24.02±3.2</td>
<td>73.25±41.6</td>
<td>73.00±1.7</td>
</tr>
<tr>
<td>F12</td>
<td>10.51±3.9</td>
<td>113.25±43.4</td>
<td>68.57±2.1</td>
</tr>
</tbody>
</table>

Data represent mean±standard deviation (SD), n=3. For particle size n=100. *CDR at 8 h.

**Fig. 1: Effect of (a) Stirring speed, (b) Evaporation time, (c) Drug/polymer ratio and (d) Aqueous/organic phase ratio on the particle size of the extract-loaded ethyl cellulose microspheres (data represent mean±SD, where n=3). SD = standard deviation**
**In vitro drug release study**

*In vitro* drug release from extract-loaded ethyl cellulose microspheres was investigated both in gastric (pH 1.2) and intestinal (pH 7.4) pH. Dissolution studies were performed for 2 h at pH 1.2 and 12 h at pH 7.4. At pH 1.2 negligible amount of drug was released from all the formulations (<8%). Whereas at pH 7.4 the maximum drug release (56.19-99.22%) indicating the sustained release pattern of the drug from microspheres. The cumulative amount of drug released (CDR) at 12 h from formulation F7-F9 with drug-polymer ratio 1:1, 1:2 and 1:3 were 99.22%, 88.3%, and 56.19% respectively. The decreased % CDR could be due to the increased particle size, resulting in the smaller surface area at high polymer concentration. Another explanation could be the high polymer concentration hinders the drug release by diffusion. Evaporation time influences the particle size and hence affects the drug release. Greater drug release was observed from the formulation F6, prepared with longer evaporation time (3h), due to smaller particle size. Rapid solvent evaporation leads to the smoother surface of the particles as compared to the particles obtained by delayed solvent evaporation. Thus the smoother surface of the particles resulted in the much slower release. Smaller particles were obtained at a high, stirring rate as high speed causes the formation of the finer dispersion of the microparticles. It was explained previously that smaller the particle size, greater the surface area, resulting in faster drug release. Maximum release (92.5%) was observed at the speed of 1500 rpm, but at 800 rpm that was 62.30% due to the formation of larger particles. Larger the particles, slower the drug release because of longer diffusion pathways that the drug had to travel to reach dissolution medium. The CDR at 12 h decreased with increasing aqueous phase volume used in the preparation of microspheres. The difference in release profiles can be attributed to the difference in the surface of the microparticles regardless of the difference in their size. The large volume of aqueous phase causes faster precipitation of the polymer, resulting in the formation of smoother and less porous surface of microparticles. Porosity increases with decreasing aqueous phase volume and thus lower organic/aqueous phase ratio resulted in a more porous surface leading to faster drug release [13, 19]. The CDR at 12 h from F10 to F12 prepared with organic/aqueous phase ratio 1:3, 1:5 and 1:10 were 88.3%, 73%, and 68.57% respectively.
Release kinetics study

The dissolution data of the optimized formulation was analyzed according to various model dependent approaches (zero order, first order, Higuchi, and Korsmeyer-Peppas) and the mode of drug release from microspheres was calculated by plotting the curves. The kinetic model with the highest value of the coefficient of determination (R2) was considered to be a more suitable model for dissolution profile. In vitro release data follows first-order kinetics (R2=0.988) followed by Higuchi model (R2=0.978). Release mechanism was studied by Peppas equation. The value of slope (n) was calculated and found to be greater than 0.89 which indicates the mode of drug release is super case II type in which the erosion of the polymer takes place to release the drug content from the matrix. The first order plot of optimized formulation was shown in fig. 5.

Fig. 4: In vitro drug release profile of optimized formulation (data represent mean±SD, where n=3). SD = standard deviation

![First order plot of optimized formulation](image)

Fig. 5: First order plot of optimized formulation

![FTIR spectra](image)

Fig. 6: FTIR spectra of (a) Extract, (b) Polymer (EC), (c) Empty microspheres and (d) Extract-loaded microspheres
Compatibility study by FTIR spectroscopy

The compatibility of the extract with the excipients in this formulation was evaluated qualitatively through FTIR analysis. The FTIR spectra obtained for pure extract, polymer, empty microspheres and extract-loaded microspheres, could confirm the chemical compatibility of extract in the ethyl cellulose microspheres. The FTIR spectrum of Syzygium cumini seed extract exhibited absorption in the range of 3404.66 cm\(^{-1}\) to 637.11 cm\(^{-1}\) (fig. 6). The spectrum showed a broad band around 3404.66 cm\(^{-1}\) assigned to alcohol and hydroxyl group (OH) stretching, which also indicated the presence of phenol and flavonoid. The sharp peak observed at 2929.14 cm\(^{-1}\) indicates the presence of alkane group (C-H). Another sharp peak at 1623.08 cm\(^{-1}\) associated with an N-H stretching (primary amines). The peaks at 1451.87 and 1363.00 cm\(^{-1}\) represent CH stretching. The sharp peak observed at 1047.98 cm\(^{-1}\) indicates the presence of aliphatic amines (C-N). The peaks observed at 921.01, 773.66 and 637.11 cm\(^{-1}\) represents C-H stretching [5]. The characteristic peaks of the extract indicate no major shift of the peak positions, matching the extract-loaded formulation spectrum. Thus the spectral analysis showed that the extract is stable in the ethyl cellulose microspheres.

Surface morphology

The SEM photograph indicates that the prepared ethyl cellulose microspheres were spherical in shape with a smooth and dense outer surface (fig. 7) without any aggregation. Distinct pores were evident on the surface of microspheres, which will be responsible for drug release.

DSC analysis

DSC studies were performed to understand the nature and interaction of the encapsulated drug in the matrix. The physical state of the drug in the polymer matrix would also influence its release characteristics [12]. DSC analysis was performed on extract, extract-loaded microspheres and the respective thermograms are shown in fig. The extract showed a characteristic peak at 259 °C, which represents the melting point of Gallic acid, but the same was not found in the thermogram of the formulation. A similar observation has been reported by [8]. These results suggested that the extract was dispersed throughout the polymer forming a high energy amorphous state.
XRD analysis

X-RD of extract and extract-loaded microspheres were carried out by using X-Ray Diffractometer to find out any change in the crystallinity of drug during microencapsulation. The x-ray diffractogram of extract showed sharp peaks, whereas the formulation decreased the sharpness of peak which indicated that the polymer dispersed the extract at molecular level blended ethyl cellulose microspheres by decreasing the crystallinity of the extract [9].

CONCLUSION

Extensive work on the formulation and characterization of extract-loaded EC microspheres was evaluated. The development of formulation and optimization yields the desired microspheres with sustained drug release for 12 h. The rheological properties exhibited that all microspheres were free-flowing in nature. SEM photographs confirmed the spherical shape of the microspheres. The results of FTIR, DSC, and XRD revealed that experimental conditions allowed a uniform distribution of the extract within EC microspheres having no significant effect on drug-polymer interaction. The particle size was found to be in the range of 34.25–176.25 µm and showed
uniform size distribution. Finally, the results of this investigation elucidate that the process and formulation variables could be effectively altered to achieve the desired characteristics of the EC microspheres for novel delivery of the herbal drug.

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AUTHORS CONTRIBUTIONS
Ranu Biswas conducted the experiment and prepared the manuscript. Dr. Kalyan Kumar Sen supervised the work and helped in manuscript preparation and correction.

CONFLICT OF INTERESTS
The authors declare that there are no conflicts of interest.

REFERENCES